PRODUCT DATA SHEET

Purolite® C100H

Polystyrenic Gel, Strong Acid Cation Resin, Hydrogen form

PRINCIPAL APPLICATIONS

• Demineralization - Industrial Water

ADVANTAGES

- Excellent physical and chemical stability
- Good kinetic performance
- High operating capacity

SYSTEMS

- Coflow regenerated systems
- Conventional counterflow systems

TYPICAL PACKAGING

- 1 ft³ Sack
- 25 L Sack
- 5 ft³ Drum (Fiber)
- 1 m³ Supersack
- 42 ft³ Supersack

TYPICAL PHYSICAL & CHEMICAL CHARACTERISTICS:

Polymer Structure	Gel polystyrene crosslinked with divinylbenzene
Appearance	Spherical Beads
Functional Group	Sulfonic Acid
Ionic Form	H ⁺ form
Total Capacity (min.)	2.0 eq/L (43.7 Kgr/ft³) (Na ⁺ form)
Moisture Retention	51 - 55 % (H ⁺ form)
Particle Size Range	300 - 1200 μm
< 300 μm (max.)	1 %
Uniformity Coefficient (max.)	1.7
Reversible Swelling, Na ⁺ → H ⁺ (max.)	9 %
Specific Gravity	1.2
Shipping Weight (approx.)	745 - 785 g/L (46.6 - 49.1 lb/ft³)
Temperature Limit	120 °C (248.0 °F)



Hydraulic Characteristics

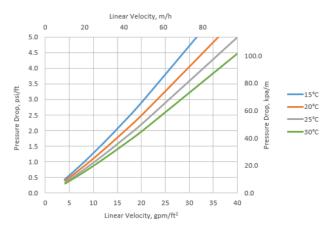
PRESSURE DROP

The pressure drop across a bed of ion exchange resin depends on the particle size distribution, bed depth, and voids volume of the exchange material, as well as on the flow rate and viscosity of the influent solution. Factors affecting any of these parameters—such as the presence of particulate matter filtered out by the bed, abnormal compressibility of the resin, or the incomplete classification of the bed—will have an adverse effect, and result in an increased head loss. Depending on the quality of the influent water, the application and the design of the plant, service flow rates may vary from 10 to 40 BV/h.

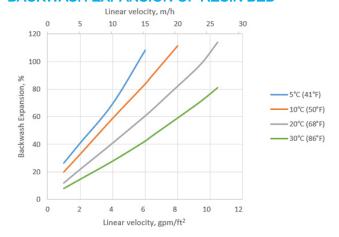
BACKWASH

During up-flow backwash, the resin bed should be expanded in volume between 50 and 70% for at least 10 to 15 minutes. This operation will free particulate matter, clear the bed of bubbles and voids, and reclassify the resin particles ensuring minimum resistance to flow. When first putting into service, approximately 30 minutes of expansion is usually sufficient to properly classify the bed. It is important to note that bed expansion increases with flow rate and decreases with influent fluid temperature. Caution must be taken to avoid loss of resin through the top of the vessel by over expansion of the bed.

PRESSURE DROP ACROSS RESIN BED



BACKWASH EXPANSION OF RESIN BED







Algeria
Australia
Bahrain
Brazil
Canada
China
Czech Republic
France

Germany

India Indonesia Israel Italy Japan Jordan Kazakhstan Korea Malaysia Mexico
Morocco
New Zealand
Poland
Romania
Russia
Singapore
Slovak Republic
South Africa

Spain Taiwan Tunisia Turkey UK Ukraine USA Uzbekistan



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